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## Editors' Choice—4D Neutron and X-ray Tomography Studies of High Energy Density Primary Batteries: Part I. Dynamic Studies of LiSOCl<sub>2</sub> During Discharge

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# Editors' Choice—4D Neutron and X-ray Tomography Studies of High Energy Density Primary Batteries: Part I. Dynamic Studies of LiSOCl<sub>2</sub> during Discharge

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## Abstract

The understanding of dynamic processes in Li-metal batteries is an important consideration to enable the full capacity of cells to be utilised. These processes, however, are generally not directly observable using X-ray techniques due to the low attenuation of Li; and are challenging to visualise using neutron imaging due to the low temporal resolution of the technique. In this work, complementary X-ray and neutron imaging are combined to track the dynamics of Li within a primary Li/SOCl<sub>2</sub> cell. The temporal challenges posed by neutron imaging are overcome using the golden ratio imaging method which enables the identification of Li diffusion *in operando*. This combination of techniques has enabled an improved understanding of the processes which limit rate performance in Li/SOCl<sub>2</sub> cells and may be applied beyond this chemistry to other Li-metal cells.

## Introduction

Lithium batteries have transformed energy storage technology due to their significant advantages in comparison to other cell chemistries, including their high cell voltage, comparatively lightweight nature of the cells, long cycle life and high capacity and rate performance. These characteristics have enabled Li cells to be deployed in applications as varied as portable electrical devices, medical implants [1], automotive powertrains [2] or for applications in space [3]. Primary Li cells have historically been preferred for long-duration backup power due to their outstanding shelf-life, high potential and capacity. One of the most common cell chemistries for such applications is the Li metal vs. thionyl chloride (SOCl<sub>2</sub>) [4–7] cell which is also suitable for applications under extreme conditions including very low or

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4 40 high temperatures [8,9]. Li-SOCl<sub>2</sub> primary batteries are mainly available in two cell designs:  
5 41 the bobbin configuration, investigated in that manuscript, and as a spirally wound cell. Bobbin  
6 42 type cells, while low cost and relatively simple to manufacture, can show a fundamental  
7 43 capacity loss at higher discharge rates. A number of different factors can prematurely interrupt  
8 44 the cell operation, such as the loss of the electrical or ionic conductivity of the electrodes. An  
9 45 improved understanding of mechanisms which lower the cell capacity and lifetime is crucial  
10 46 for designing improved batteries.

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15 47 Three-dimensional (3D) and four-dimensional (4D) imaging, i.e. 3D spatially and temporally  
16 48 resolved methods such as X-ray computed tomography (CT), are powerful tools to track  
17 49 processes which affect battery performance. The high spatial and time resolution which range  
18 50 from the millimetre to the nanometre length scale [10], exposure times of fractions of a second  
19 51 to acquire radiographic images [11,12] and as little as several seconds for full CTs [13–15]  
20 52 enable the study of the battery architecture, electrode microstructure, new battery materials and  
21 53 battery safety. The high sensitivity to high-Z elements provides a good imaging contrast for  
22 54 metallic materials such as the anode and cathode current collectors, and the active electrode  
23 55 materials such as LiMnO<sub>2</sub> [15], LCO [16], LFP [17] or NMC [18]. However, light elements  
24 56 such as lithium appear transparent when imaged with X-rays, in the ‘tender’ or hard X-ray  
25 57 energy spectrum. In contrast, neutrons show a high sensitivity for some low-Z elements  
26 58 providing a high contrast for both lithium and hydrogen. In contrast, some metals such as lead  
27 59 have low attenuation coefficients when imaged using neutrons. This is a consequence of X-  
28 60 rays interacting with the electron cloud with the attenuation coefficient increasing with a rising  
29 61 Z, whereas neutrons interact with the nucleus and provide different attenuation coefficients  
30 62 even between isotopes of the same element. Recently, neutron tomography has demonstrated  
31 63 significant potential in imaging electrochemical devices, for example, for visualising the water  
32 64 evolution in fuel cells [19–21] and electrolyzers [22,23], to examine dynamic Li diffusion  
33 65 processes and electrode expansion [24–27], electrolyte consumption [28] and gas evolution  
34 66 [29–31] in Li batteries. However, neutron imaging is often limited to radiography and suffers  
35 67 from poor spatial resolution and long exposure times due to the characteristically low flux  
36 68 available at most neutron sources. This makes it challenging to image dynamic processes at  
37 69 high-resolution. Recent developments have shown an improved speed in neutron CT collection  
38 70 [32,33] and spatial resolutions down to a few micrometres [34–36] are achievable, which in  
39 71 turn has increased the potential to track dynamic lithium diffusion processes in lithium batteries.  
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54 72 In cases where dynamic processes are slow, neutron sources with a lower flux can perform 4D  
55 73 studies by using an appropriate spatiotemporal scanning strategy, such as the golden-ratio (GR)  
56 74 scanning method. Conventional tomographic reconstruction techniques require projections in  
57 75 sequences of equal angular distances. The spatial and temporal resolution is predetermined and  
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cannot be changed during the measurements or afterwards. Additionally, if one of the sequential projections is missing or defective, caused by problems with the camera system or an interruption of the radiation, the data cannot be reconstructed or will contain significant artefacts. In the case of a static sample the missing projections can be repeated, or fluctuations of the neutron flux can be monitored and balanced by the variation of the exposure time. However, replacing lost projections is not possible for dynamic processes. The mathematical background and a demonstration of the GR technique is shown by Kaestner *et al.* [37]. This scanning strategy is based on non-sequential decompositions of the sample rotation angle sequence. The organisation of the projections by using the golden-ratio was first introduced by Köhler [38], who organised the projections by using the GR (shown in Equation 1) to calculate the optimal acquisition angle of each projection such as shown in Equation 2 for a tomographic scan over  $180^\circ$  with  $n$  the number of the projections.

$$g = \frac{\sqrt{5} - 1}{2} \approx 0.618 \quad \text{Equation 1}$$

$$GR \text{ angle } (n) = g \cdot n \cdot 180^\circ \bmod 180^\circ \mid n \in \mathbb{Z}_0^+ \quad \text{Equation 2}$$

The next angle is centred in the biggest gap of the previously acquired angles to minimise the overlap of the completed projections and prevent redundant information. Using this method, a time-resolved data set is achieved by using a certain set of consecutive projections, possibly with a high overlap of the projections between consecutive tomographies in a running-average mode. For an improvement in spatial resolution, a larger number of consecutive projections is used and the projection overlap can be reduced.

The combination of both non-destructive neutron and X-ray CT techniques provides opportunities to combine structural information such as particle movements, obtained from the X-rays, with electrochemical information such as lithium diffusion or the lithium content change in the cathode or anode, obtained from the neutrons. The successful combination of X-ray and neutron CT on batteries was for the first time demonstrated by LaManna *et al.* [39]. This combination of complementary imaging techniques enables the study of the dynamic processes inside batteries in 4D and provides opportunities to deliver new insights in processes which occur simultaneously such as e.g. Li diffusion and electrode expansion [40].

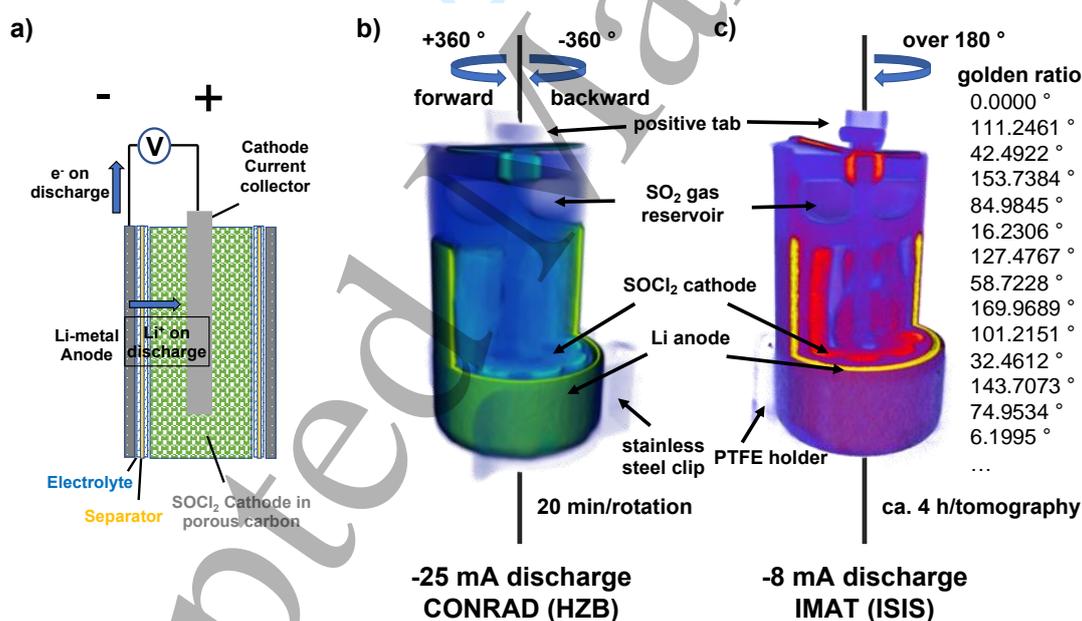
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### 103 **Experimental**

104 1200 mAh LS 14250 Li-SOCl<sub>2</sub> cells (Saft Groupe A.A., France) were examined to understand  
105 the rate-dependent structural changes using a combination of X-ray and neutron imaging. The  
106 LS 14250 cell is a ½ AA sized commercial Li/SOCl<sub>2</sub> battery with an internal bobbin type  
107 structure designed for low-rate applications such as backup batteries in computers or burglar  
108 alarm systems. This low-cost, primary cell type provides a nominal voltage of 3.6 V at room

109 temperature with a flat discharge profile over a long-time range and can operate over a wide  
 110 temperature range of  $-60$ – $85$  °C, with a very low self-discharge rate, which makes the cell  
 111 chemistry a popular choice for applications in extreme conditions [5,41]. Figure 1(a) shows the  
 112 schematic drawing of the internal structure of a bobbin type Li/SOCl<sub>2</sub> battery cell. The liquid  
 113 SOCl<sub>2</sub> cathode (green) in the middle of the cell is surrounded by the lithium-metal negative  
 114 electrode (grey) and separated by a separator layer (yellow) soaked in a SOCl<sub>2</sub>:LiAlCl<sub>4</sub> non-  
 115 aqueous electrolyte (blue). A porous supporting carbon skeleton surrounds the liquid cathode  
 116 providing an enhanced electrical conductivity. A cathode current collector rod (grey) in the  
 117 centre of the cell connects this porous carbon to the positive tab. The lithium anode is directly  
 118 connected to the cell can which acts as the negative terminal. During cell discharge Li-ions  
 119 move from the Li anode into the electrolyte, diffuse through the Li<sup>+</sup> permeable separator layer  
 120 to the cathode side and react with the SOCl<sub>2</sub> to form LiCl, SO<sub>2</sub> gas and solid sulphur.

121 Two LS 14250 cells were discharged under constant current conditions at 25 mA and 8 mA,  
 122 respectively. Both of these discharge currents are below the maximum recommended discharge  
 123 current of 35 mA, however, these rates are known to result in a significant loss of usable  
 124 capacity, as detailed in the cell data sheet.



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 126 Figure 1 (a) schematic illustration of a Li-metal/thionyl chloride bobbin type cell (b) 3D reconstruction of a LS14250 cell discharged  
 127 at 25 mA while being scanned on the CONRAD-2 neutron imaging beamline with sequences of equal angular projections in forward  
 128 and backward rotation through 360° and (c) 3D reconstructions of a LS14250 cell discharged at 8 mA scanned on the IMAT beamline  
 129 with the GR decomposition strategy. The first projection angles for the GR scan are listed on the right hand side.

130 Time resolved neutron CT scans at a 25 mA discharge current were performed at the V7  
 131 CONRAD-2 neutron imaging beamline [42,43] at the BER II research reactor at the Helmholtz  
 132 Zentrum Berlin. CONRAD-2 is optimised for high spatial and time resolved neutron imaging.

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4 133 The intermediate measuring position of CONRAD-2 was used to maximize the high neutron  
5 134 flux at an acceptable spatial resolution. This position was equipped with a high speed, indirect  
6 135 detector system including a 200  $\mu\text{m}$  thick  $^6\text{LiF/ZnS:Ag}$  scintillator screen for a high neutron to  
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8 136 light conversion efficiency and a cooled  $-30\text{ }^\circ\text{C}$  sCMOS 'Neo' camera from Oxford  
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10 137 Instruments/Andor (UK) which provides a high frame rate with short readout delays. Both  
11 138 components were used in combination with a bright Nikon photo lens ( $f=50\text{ mm}$ , aperture 1.2)  
12 139 to reduce the light losses inside the camera box and focus the object on to the camera photo  
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14 140 chip. For an optimal L/D ratio a 3 cm pinhole configuration was selected, positioned about 5 m  
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16 141 in the front of the detector system at the end of the NL-1B neutron guide. The LS 14250 cell  
17 142 was mounted in front of the scintillator screen on an adjustable stick on the V7 rotation stage  
18 143 (Goniometer 409, Huber Diffraktionstechnik, Germany) by a stainless steel clip. With a  
19 144 calculated L/D of about 167, the spatial resolution was about  $150\text{ }\mu\text{m}$  with a pixel size of  $55\text{ }\mu\text{m}$ .  
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21 145 Before the cell was secured onto the sample holder the plastic coating was removed to mitigate  
22 146 the contribution of this layer to neutron scattering. The electrical connection to the GAMRY  
23 147 1000E potentiostat (GAMRY Instruments, USA) was maintained by a stainless steel clip at the  
24 148 electrical negative cell can and a crocodile clip at the top positive terminal tab. The battery was  
25 149 discharged in constant current mode at 25 mA. During discharging, continuous neutron  
26 150 radiographies were collected with an exposure time of 2 s per image by the Andor Solis  
27 151 software. Tomograms were sequentially accumulated during  $360^\circ$  rotation with 600 projections  
28 152 acquired for each full tomography in approximately 20 mins. Every hour, two tomographies  
29 153 were performed whereby the first was acquired through a counter-clockwise rotation and the  
30 154 second clockwise; labelled as forward and backward respectively. Figure 1(b) shows an  
31 155 example of a 3D data set with an illustration of the rotation conditions. After every second  
32 156 tomography, the battery was translated out of the beam to collect open beam and dark field  
33 157 images to enable the correction and normalisation of the projections. For data processing the  
34 158 'Remove Outliers' and median filter of ImageJ Fiji [44] were used to remove white spots which  
35 159 are caused by fast neutrons and gamma radiation from the 16-bit images. Reconstruction of the  
36 160 tomographies was performed using the Octopus 8.9 software (XRE, Gent, Belgium) using the  
37 161 filtered back projection (FBP) reconstruction algorithm. Due to the high neutron absorption of  
38 162 lithium, the reconstructed slices were then corrected for beam hardening using the first  
39 163 tomogram to determine the parameters which are utilised for all following tomograms. The  
40 164 parameters are optimised in such a way that the lithium anode and the  $\text{SOCl}_2$  cathode, in the  
41 165 middle of the cell, show a homogeneous attenuation coefficient respectively. Throughout the  
42 166 experiment 47 full tomograms were collected, 24 in forward and 23 in backward rotation with  
43 167 the process taking ca. 20.3 h and the battery providing a capacity of 506 mAh.

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59 168 A second 4D neutron imaging scan with an 8 mA discharge current was performed on the IMAT  
60 169 neutron imaging beamline [45–47] at the ISIS neutron spallation source. In contrast to most

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3 170 reactor based neutron sources, neutron spallation sources such as the ISIS neutron source at the  
4 171 Rutherford Appleton Laboratory (UK) have a lower time-averaged neutron flux which makes  
5 172 imaging of dynamic processes with the conventional scanning strategies more difficult. To  
6 173 overcome this challenge, methods such as the Golden Ratio (GR) strategy can be employed.  
7 174 Using this method, the sample is imaged at non-regular intervals with the organisation of the  
8 175 angular distribution calculated by the GR. This method can be used for angular ranges of  $\pi$  or  
9 176  $2\pi$  with each consecutive scanning angle minimising the overlap of the previously scanned  
10 177 projections avoiding the acquisition of redundant information. GR projections are acquired  
11 178 continuously, over a chosen experimental period, enabling the optimisation of either the  
12 179 temporal or spatial resolution by post-image processing by selecting the number of projections  
13 180 from the GR tomogram that are reconstructed. By ensuring an overlap of the projections of  
14 181 consecutive tomographies in the projection sequence (i.e. taking a 'running average') an  
15 182 improved time resolution is achieved. As the neutron flux at the ISIS spallation source is  
16 183 approximately  $10\times$  lower than at CONRAD-2 for the same L/D ratio, the GR decomposition  
17 184 strategy was applied here. An indirect detector box with a  $80\ \mu\text{m}$  thick  ${}^6\text{LiF/ZnS:(Cu/Ag)}$   
18 185 scintillator (Tritec, Switzerland) in combination with a Nikon photo lens ( $f=135\ \text{mm}$ , aperture  
19 186 2) and an ANDOR Zyla sCMOS 4.2 PLUS camera (Oxford Instruments Andor, UK) was  
20 187 utilised. The box was adjusted to a pixel size of  $29\ \mu\text{m}$  with a pinhole size of  $40\ \text{mm}$  with a  
21 188 L/D ratio of ca. 250 which achieved a spatial resolution of about  $80\ \mu\text{m}$ . Once more, the plastic  
22 189 cover of the LS 14250 battery cell was removed, before the cell was inserted in a neutron  
23 190 transparent cylindrical PTFE sample holder. Electrical connections were maintained by  
24 191 attaching a copper cable between the negative battery can and the PTFE wall and attaching a  
25 192 crocodile clip to the positive battery tab. The PTFE holder was screwed to an adapter rod which  
26 193 was mounted onto a Huber Goniometer 411 (HUBER Diffraktionstechnik, Germany) rotation  
27 194 stage and positioned close to the camera box. Due to the limited rotation angle between  $0^\circ$  and  
28 195  $180^\circ$  no specialised cable connection such as a slip ring was needed. Owing to the low neutron  
29 196 flux, a long exposure time of 30 s was used to maximise counting statistics. A GAMRY 1000E  
30 197 potentiostat discharged the cell at a constant current mode of 8 mA during the scan. The angular  
31 198 distribution for the whole scan was calculated using the GR with Figure 1(c) showing a 3D  
32 199 reconstruction of the partially discharged cell and the first calculated GR projection angles over  
33 200 an angular range of  $\pi$ . In advance of the discharge scan of the cell, a 4 h tomography was  
34 201 acquired to enable a full reconstruction of the cell in pristine condition. After every 610  
35 202 projections the cell was moved out of the beam for five open beam images to facilitate image  
36 203 correction after all the projections had been acquired. The total discharging process took about  
37 204 104 h, after which the cell had delivered a capacity of 832 mAh. After correcting each  
38 205 projection using the dark and open beam images, and after filtering white spots, 3D  
39 206 reconstructions were performed *via* the FBP algorithm for a parallel beam using the ASTRA

207 toolbox [48,49] reconstruction library within the python programming language. For the  
208 number of projections, the Fibonacci number 377 was utilised due to a better reconstruction  
209 result in combination with a shift of 188 projections for each following reconstruction. This  
210 results in an overlap of 189 projections and a time shift of about 2 h between the tomographies.

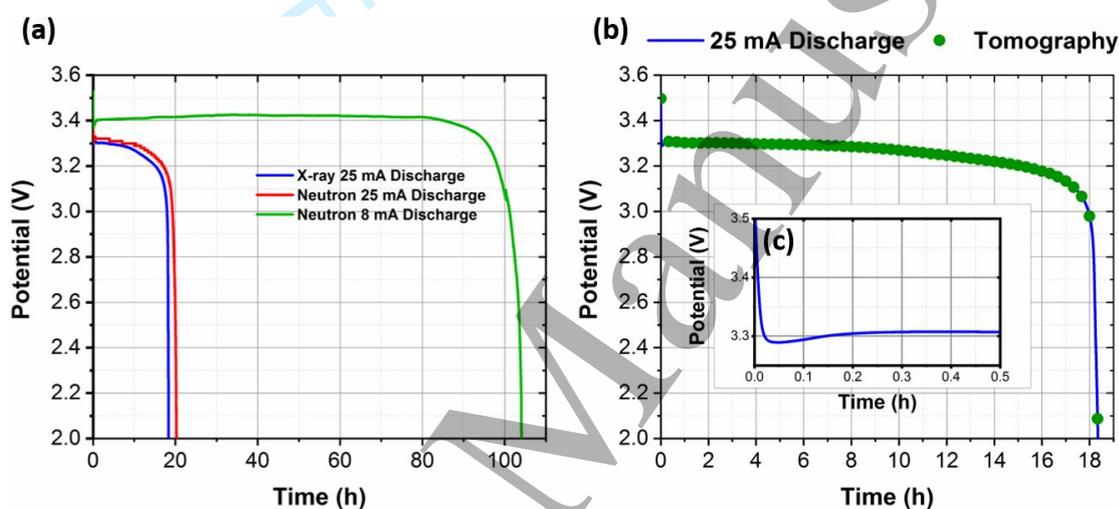
211 Four dimensional X-ray tomography was achieved on a Nikon XTH 225 laboratory X-ray  
212 system (Nikon Corporation, Japan) using a 225 kV reflection target source with a focal spot  
213 size of 3  $\mu\text{m}$  at 7 W. A PerkinElmer 1620 16-bit (PerkinElmer Inc. USA) detector with a  
214  $2000 \times 2000$  pixel array and a pixel size of 200  $\mu\text{m}$  was used to capture all images. The plastic  
215 cover of the cell was removed prior to mounting the cell with double-sided tape onto the sample  
216 holder of the rotation stage. An electrical connection was maintained by applying a crocodile  
217 clip to the positive tab, with the negative connection achieved by connecting a copper cable to  
218 the cell can using insulating tape. Both cables were then connected to an electrical slip ring (P4  
219 + Compact Slip Ring, Moog, UK) which allowed a continuous rotation of the stage without  
220 losing the electrical connection. The battery was discharged using a GAMRY 1000E  
221 potentiostat (GAMRY Instruments, USA) in constant current mode with a discharge current of  
222 25 mA. The instrument was programmed to continuously collect projections at an X-ray tube  
223 voltage level of 120 kV and current of 140  $\mu\text{A}$ . To achieve one full tomogram, 1201 projections  
224 were captured through an angular range of  $360^\circ$  with an exposure time of 1 s per projection,  
225 leading to a total image acquisition time of ca. 20 mins. The total cell discharge took about  
226 18.3 h and reached a capacity of 459 mAh which enabled the capture of 56 full tomographies  
227 of the cell during discharge. The tomograms were reconstructed using the FDK (FDK\_CUDA)  
228 circular cone beam reconstruction algorithm from the ASTRA toolbox [48,49] reconstruction  
229 library within the python programming language. Before starting the 3D reconstruction, the  
230 projections were corrected by the dark field and open beam images which were collected before  
231 and after the scan and binned by a factor of two to reduce the reconstruction time and data size  
232 resulting in a reconstructed pixel size of 40.4  $\mu\text{m}$ .

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## 234 **Results and Discussion**

235 As shown in Figure 2(a) the discharge curves of all three discharged LS 14250 cells show the  
236 typical flat discharge profiles at a high potential expected for the Li/SOCl<sub>2</sub> chemistry. The cells  
237 operated at the higher discharge current of 25 mA display a lower potential plateau at ca. 3.3 V  
238 with the cell discharged at 8 mA exhibiting a slightly higher potential plateau in excess of 3.4 V.  
239 At the beginning of the discharging process, the voltage delay, characteristic of Li/SOCl<sub>2</sub> cells,  
240 can be seen to be shorter for the cell discharged at a higher current requiring ca. 0.5 h before  
241 the potential is stabilised [Figure 2(c)]. In comparison, a long delay of about 30 h is observed  
242 for the low current discharge in Figure 2(a). This initial voltage delay occurs in Li/SOCl<sub>2</sub> cells

243 due to the formation of a passivating LiCl layer at the anode during cell storage. The increased  
 244 time needed to recover the normal potential of the cell observed during the low discharge is  
 245 due to a reduced level of mechanical disruption, which removes the passivation layer on the  
 246 lithium metal surface [50]. At the point the voltage recovers to a plateaued voltage the whole  
 247 Li-metal surface can participate in the discharge reaction. The slightly lower potential of the  
 248 cell scanned with X-ray compared to the one scanned with neutrons is attributed to  
 249 manufacturing variations. The difference in cell capacity of 459 mAh compared to 506 mAh  
 250 may be a result of a higher self-discharge during a longer cell storage time, or differences in  
 251 the active mass loading during manufacture. Internal mechanisms in the cell such as the  
 252 shielding of active electrode material by a SO<sub>2</sub> gas layer on the Li-metal surface can result in  
 253 similar effects.



254  
 255 **Figure 2** (a) Discharge curves of the three LS14250 cells used in this work, two discharged at 25 mA scanned with X-rays and neutrons  
 256 and one cell at 8 mA imaged with neutrons (b) A detailed discharge curve of the cell discharged at 25 mA scanned with X-rays. Green  
 257 dots mark the times when tomograms were recorded. (c) a magnified view of the voltage delay at the beginning of the cell discharging  
 258 process, typical for Li/SOCl<sub>2</sub> chemistry.

259 Laboratory X-ray scanners or synchrotron imaging beamlines in the intermediate or lower hard  
 260 X-ray energy regime show lithium metal or lithium diffusion in a lithium battery cell only  
 261 indirectly by a grey value increase in the electrode, where the lithium is removed and a grey  
 262 value reduction where lithium is deposited. This behaviour is visible for the LS 14250 cell  
 263 scanned with X-rays in Figure 3, which shows horizontal and vertical slices of the pristine, half  
 264 discharged and fully discharged cell. The metallic battery components such as the positive tab,  
 265 the negative cell can and the cathode current collector are clearly visible, with the battery  
 266 header somewhat obscured due to reconstruction artefacts. Furthermore, the liquid SOCl<sub>2</sub>  
 267 cathode in the middle of the cell can be seen; however, the SOCl<sub>2</sub>:LiAlCl<sub>4</sub> electrolyte is not  
 268 distinguishable from the liquid cathode. Regions which are filled with an excess of electrolyte

are expected in this cell type and can be seen above the active cell material by a reduction of the electrolyte volume and an increase of the gas volume in the battery head during the discharge. The lithium metal anode is indirectly visible by the transparent region at the outer cell radius between cathode and the stainless steel cell can. The removal of lithium from the electrode is indirectly detected during the discharge process. A contrast change inside the  $\text{SOCl}_2$  cathode is not detected. During the discharging process  $\text{SO}_2$  gas is formed from the reaction of lithium with  $\text{SOCl}_2$  which is visible as bright purple areas due to a low attenuation coefficient, which is similar to air. Shortly after the initiation of the discharge process, the  $\text{SO}_2$  gas forms bubbles in the cathode which diffuse into four gas channels, which work as gas guides in the porous carbon mesh, and accumulate inside the cell header where a further gas reservoir is located. This transfer of  $\text{SO}_2$  gas away from the cathode is designed to prevent the stagnation of lithium diffusion and subsequent passivation of the anode surface during the discharge. A distinction between the evolved  $\text{SO}_2$  gas and the lithium metal is not possible in the X-ray image, because the greyscale values cannot be sufficiently differentiated.

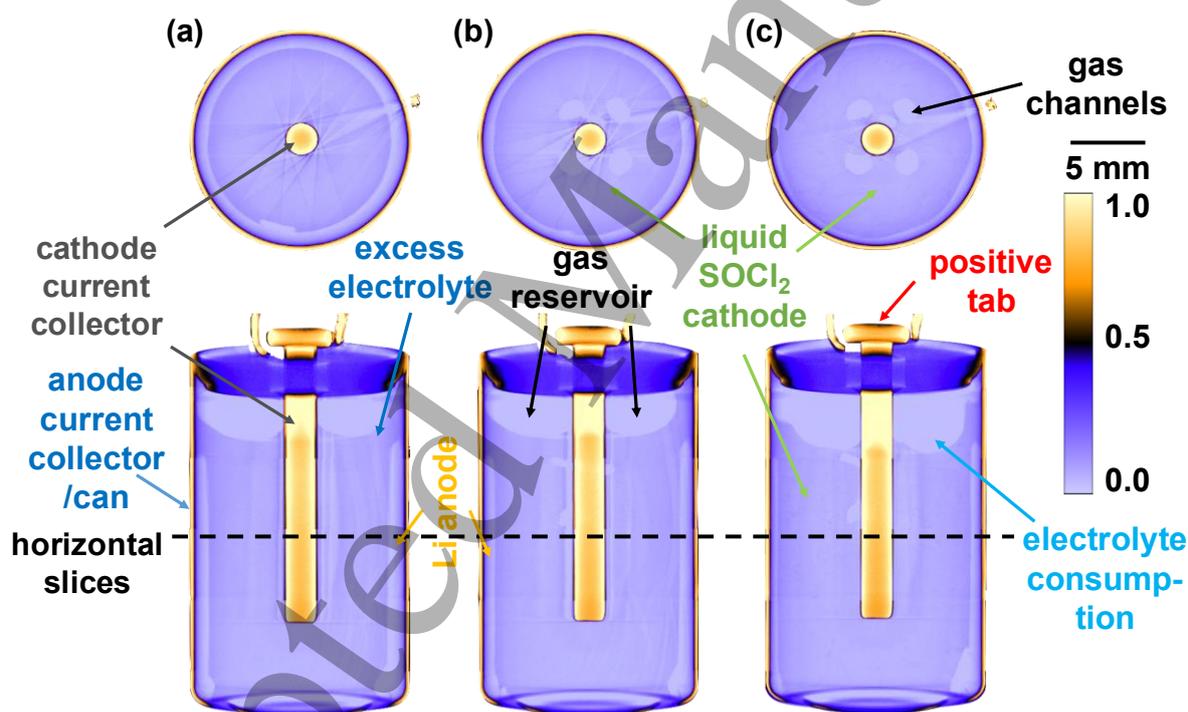


Figure 3: Orthogonal slices from the 4D X-ray scan of the LS14250 battery cell discharged at 25 mA, showing horizontal and vertical orthogonal slices from the in operando X-ray scan at three different SoCs; pristine, half discharged and the fully discharged cell.

To provide a better understanding of the processes involved in the discharge of the cell, including the removal of Li from the metal anode and the diffusion process inside the  $\text{SOCl}_2$  cathode, complementary neutron imaging was used. Time resolved neutron tomography mitigates the challenges associated with X-ray imaging discussed previously, and due to the high sensitivity of neutrons to lithium, a quantitative description of the Li removal from the

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4 291 anode and the diffusion of Li inside the thionyl chloride cathode can be achieved. Figure 4  
5 292 shows orthogonal slices obtained on CONRAD-2 from the cell discharged at 25 mA: in pristine  
6 293 condition, halfway through discharge and fully discharged, at which point the cell had delivered  
7  
8 294 a capacity of 506 mAh. In contrast to the X-ray tomographies, neutrons exhibit just a weak  
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10 295 attenuation by the metallic cell components such as the stainless steel container or the positive  
11 296 battery tab. As seen in Figure 4, the Ni, cathode current collector exhibits a similar neutron  
12 297 attenuation to the surrounding liquid  $\text{SOCl}_2$  cathode and is difficult to distinguish. However, as  
13 298 the Li content in the cathode increases, the current collector becomes more visible. More highly  
14 299 attenuating cell components, such as the boron containing glass seal which shields the  
15 300 environment from the toxic  $\text{SO}_2$  gas and the Li, are shown in bright yellow colours. As  
16 301 previously shown in the X-ray images (Figure 3), a contrast difference between the electrolyte  
17 302 and the liquid cathode in the pristine state is not observed, however, as the discharge process  
18 303 progresses the cathode can be clearly distinguished from the electrolyte due to the increase of  
19 304 the attenuation coefficient indicated by the colour change from purple to black to yellow. The  
20 305 volume reduction in the excess electrolyte in the battery header becomes visible as the  
21 306 discharge progresses, exposing the 'flower' like shapes of the supporting porous carbon  
22 307 skeleton alongside the four gas channels in the horizontal orthoslices. During the discharge  
23 308 process, Li is progressively removed from the metal anode around the cathode and diffuses  
24 309 through the separator membrane, (which is not visible due to insufficient spatial resolution),  
25 310 into the cathode. Here, the attenuation coefficient increases steadily, seen by an increase in  
26 311 contrast starting from the cathode border. As more Li moves into the cathode a high contrast  
27 312 gradient from the cathode edge into the middle of the cell can be seen. This is indicative of a  
28 313 slow lithium diffusion rate inside the cathode. At the same time,  $\text{SO}_2$  gas, which is neutron  
29 314 transparent, evolved through the discharge reaction and is marked through an increase of lowly  
30 315 attenuating regions in Figure 4. Towards the edge of the cathode, a larger volume of gas is  
31 316 generated due to the higher Li concentration in close proximity to the anode and consequent  
32 317 increased reactivity in this region. Not all of this gas diffuses into the gas channels and fills the  
33 318 gas reservoir, with a portion diffusing through the electrolyte and, in places, covering the  
34 319 surface of the anode, highlighted by green boxes in the slices in Figure 4. Such 'gas shielded'  
35 320 Li surface areas cannot participate in the chemical reaction. As a result of the slow lithium  
36 321 mobility in the cathode and the shielding of fresh lithium from the anode by gas the cell  
37 322 performance is inhibited through a reduction in both the cell capacity and operating potential.  
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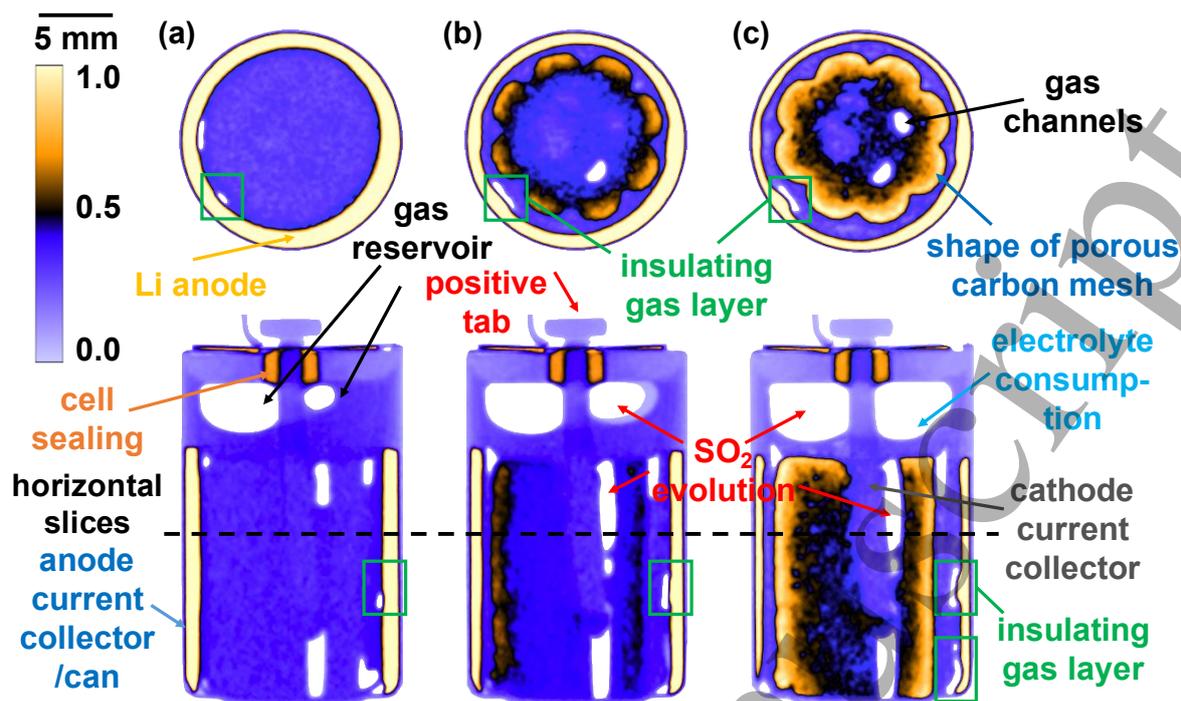
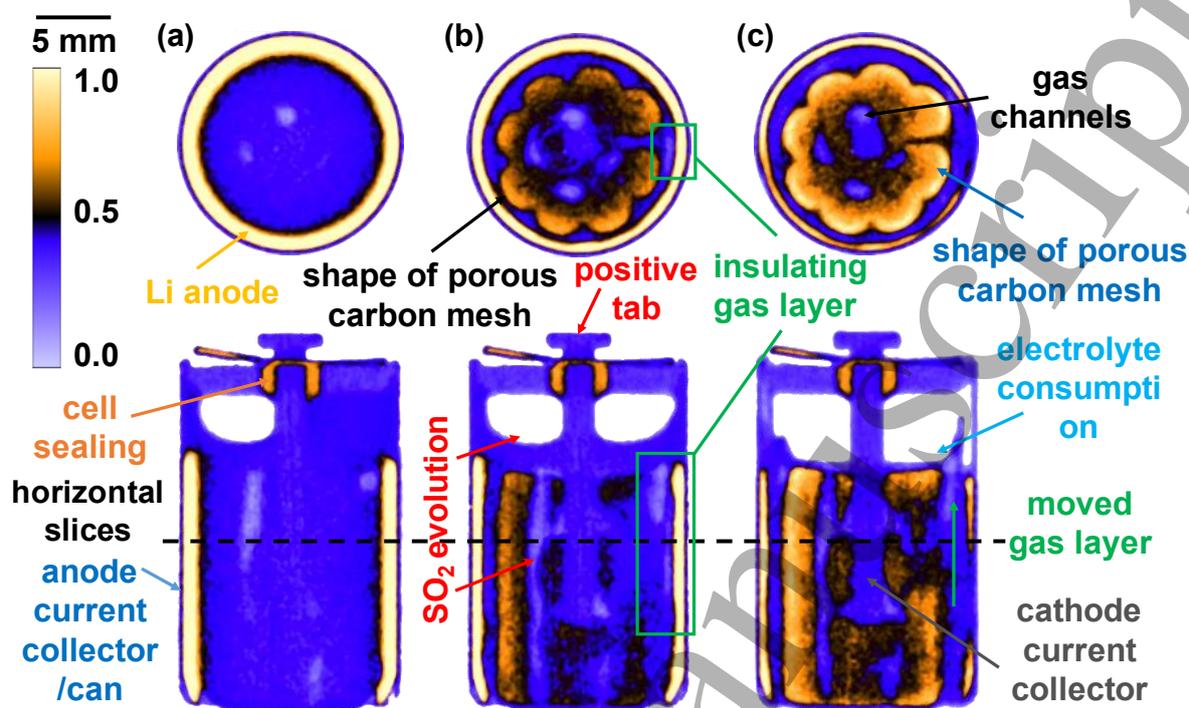


Figure 4: Orthogonal slices from the in-operando 3D neutron experiment of the LS14250 cell discharged at 25 mA at the CONRAD-2 neutron imaging beamline at three different SoCs: pristine, half discharged and fully discharged cell.

The second neutron imaging experiment provided data on a similar LS 14250 cell which was discharged at a lower discharge current of 8 mA. Orthogonal slices of three tomographies from IMAT are displayed in Figure 5, with slices from the pristine cell, in a half discharged condition and the fully discharged state with the cell yielding a total capacity of 832 mAh. The cell shows a similar discharge behaviour to that discharged at 25 mA, however, due to the lower discharge current the cell provided a ca. 40 % increase in capacity. This resulted in an increase in the consumption of lithium as seen in Figure 5, with the inhomogeneity of the lithium removal throughout the cell being particularly notable. The horizontal slices in Figure 5 initially show a homogeneous Li-metal anode in the pristine state and with the highly attenuating layer being preferentially removed towards the lower half and right hand side of the cell during discharge. This inhomogeneous Li consumption is likely caused by a misalignment of the cathode which is seen to be closer to the lower right anode side providing a shorter path to the cathode. Furthermore, evidence of the ability for gas to diffuse in this right hand region is shown in the tomograms with an area of gas evident at the surface of the anode observed when the cell is half-discharged not being present on full discharge. The lower discharge current used here also influences the quantity and depth of diffusion of Li in the cathode, which increases at lower operating currents due to the slow Li diffusion process in  $\text{SOCl}_2$ . This increased Li diffusion inside the cathode is likely the key reason for the improved cell capacity observed in this instance. At higher discharge currents, an increasing amount of lithium reacts in the outer

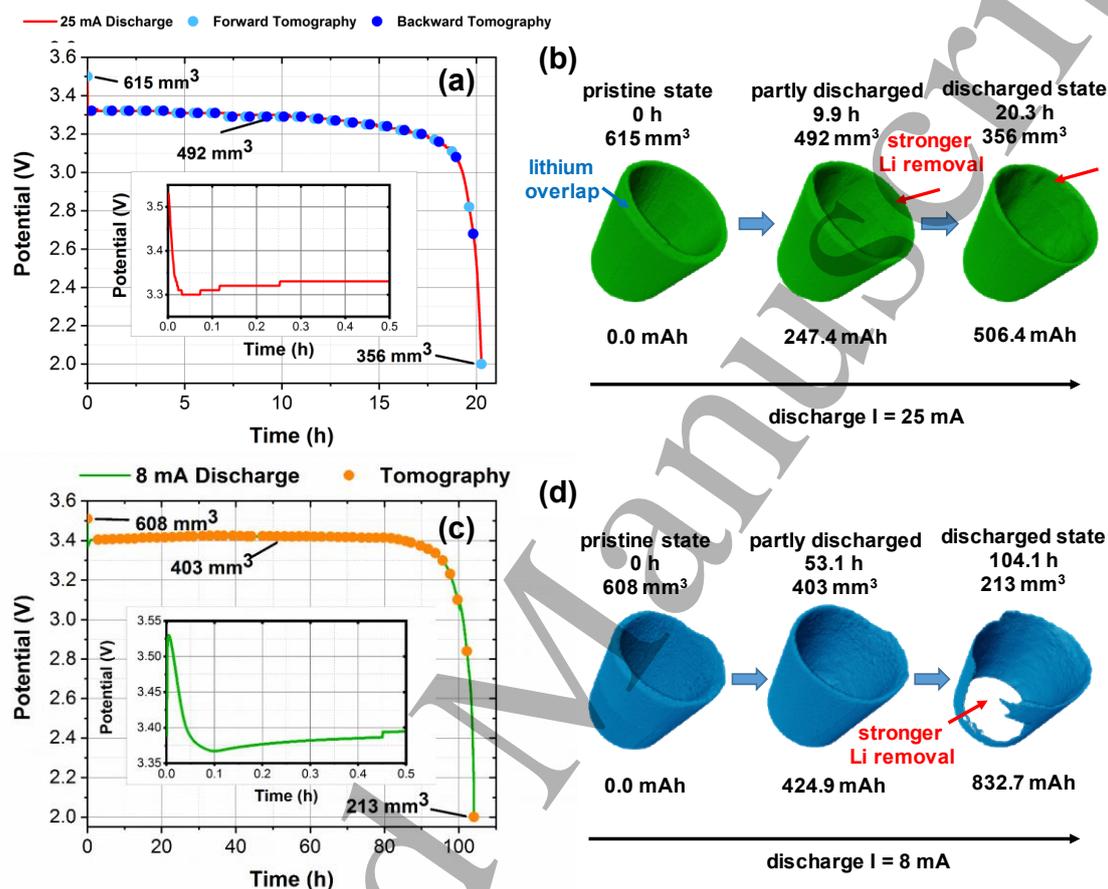
345 cathode region, forming insulating solid sulphur, which is deposited in the channels of the  
 346 porous carbon skeleton blocking the gas diffusion channels and ultimately insulating the  
 347 internal cathode where fresh  $\text{SOCl}_2$  is available, thereby reducing the cell capacity.



348  
 349 **Figure 5** Orthogonal slices from the in-operando 3D neutron experiment of the LS14250 cell discharged at 8 mA at the IMAT neutron  
 350 imaging beamline at three different SoCs; pristine, half discharged and fully discharged cell.

351 By taking advantage of the high sensitivity of neutrons to Li shown previously, a quantitative  
 352 determination of the Li-anode volume over the discharge time is possible. Here, a constant  
 353 threshold segmentation of the bright lithium anode was achieved by using the AVIZO  
 354 visualisation software suite (Thermo Fisher Scientific, USA) with the results shown alongside  
 355 the discharge curves in Figure 6. In the case of the battery cell discharged at 25 mA, the 24  
 356 tomographies measured in the forward rotation direction were used for the segmentation. Three  
 357 of the segmented volumes are visualised in Figure 6(b). In the pristine state a total Li volume  
 358 of  $615 \text{ mm}^3$  was measured with  $356 \text{ mm}^3$  remaining after the discharge process was complete.  
 359 The anode shows a flat and homogeneous inner and outer surface area in the pristine state.  
 360 During the discharge process progressive lithium removal is clearly visible at the internal  
 361 electrode in the shape of vertical stripes. These stripes are located directly opposite the bulges  
 362 of the ‘flower’ shaped cathode seen in Figure 4 and Figure 5. The shorter distance between the  
 363 electrodes at these locations facilitates increased Li removal from the anode. The overlap of  
 364 the Li-metal at the left side of the segmented anode, caused by the manufacturing process, is  
 365 also visible with a shift in height between both endings.

367 While the initial Li volume of the cell discharged at 8 mA is similar ( $608 \text{ mm}^3$ ) the Li volume  
 368 change is more substantial, with  $213 \text{ mm}^3$  remaining in the fully discharged state. Here, the Li  
 369 anode volume was determined for every second tomography. No overlap of the lithium metal  
 370 foil endings is visible which may be a result either of better initial fabrication or insufficient  
 371 spatial resolution. During the discharge process more lithium is consumed owing to the lower  
 372 discharge current, resulting in the complete removal of Li at one side of the anode.

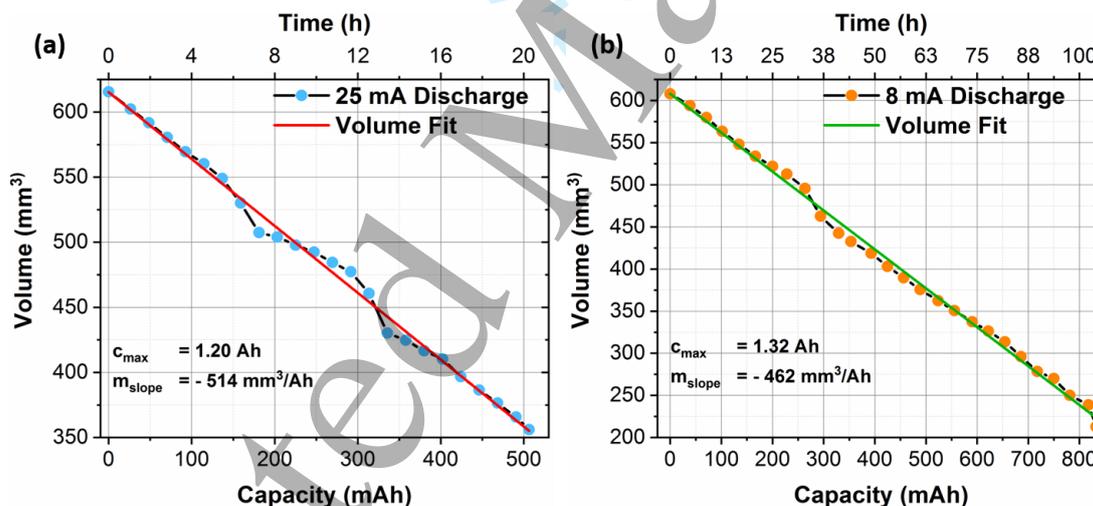


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 374 **Figure 6:** Discharge curve of the LS14250 cell discharged at (a) 25 mA and (c) 8 mA alongside volume renderings of the anode volumes  
 375 of the cells discharged at (b) 25 mA and (d) 8 mA at different SoCs with the pristine, half and fully discharged state:

376 Quantification of this Li volume decrease is achieved by correlating the volume of Li at a given  
 377 time to the capacity provided by the cell with this relationship following a linear trend as  
 378 observed in Figure 7. The initial Li metal volumes of  $615 \text{ mm}^3$  and  $608 \text{ mm}^3$ , which correspond  
 379 to a Li mass of ca.  $0.32 \text{ g}$  per cell (based on a Li density at  $20 \text{ }^\circ\text{C}$  of  $0.534 \text{ g cm}^{-3}$ ), are in a good  
 380 agreement with the manufacturer's data sheet values of approximately  $0.3 \text{ g}$  per cell. The  
 381 theoretical relationship between the used Li volume in  $\text{mm}^3$  and the resulting capacity delivered  
 382 in Ah is given in Equation 3. Here,  $M_{\text{Li}}$  corresponds to the molar mass of lithium,  $C$  the electric  
 383 charge,  $N_{\text{A}}$  the Avogadro constant and  $\rho_{\text{Li}}$  the density of lithium.

$$\left[ \frac{\text{mm}^3}{\text{Ah}} \right] = \frac{M_{\text{Li}} \cdot 3600 \left[ \frac{\text{s}}{\text{h}} \right]}{C \cdot N_A \cdot \rho_{\text{Li}}} = 485 \frac{\text{mm}^3}{\text{Ah}} \quad \text{Equation 3}$$

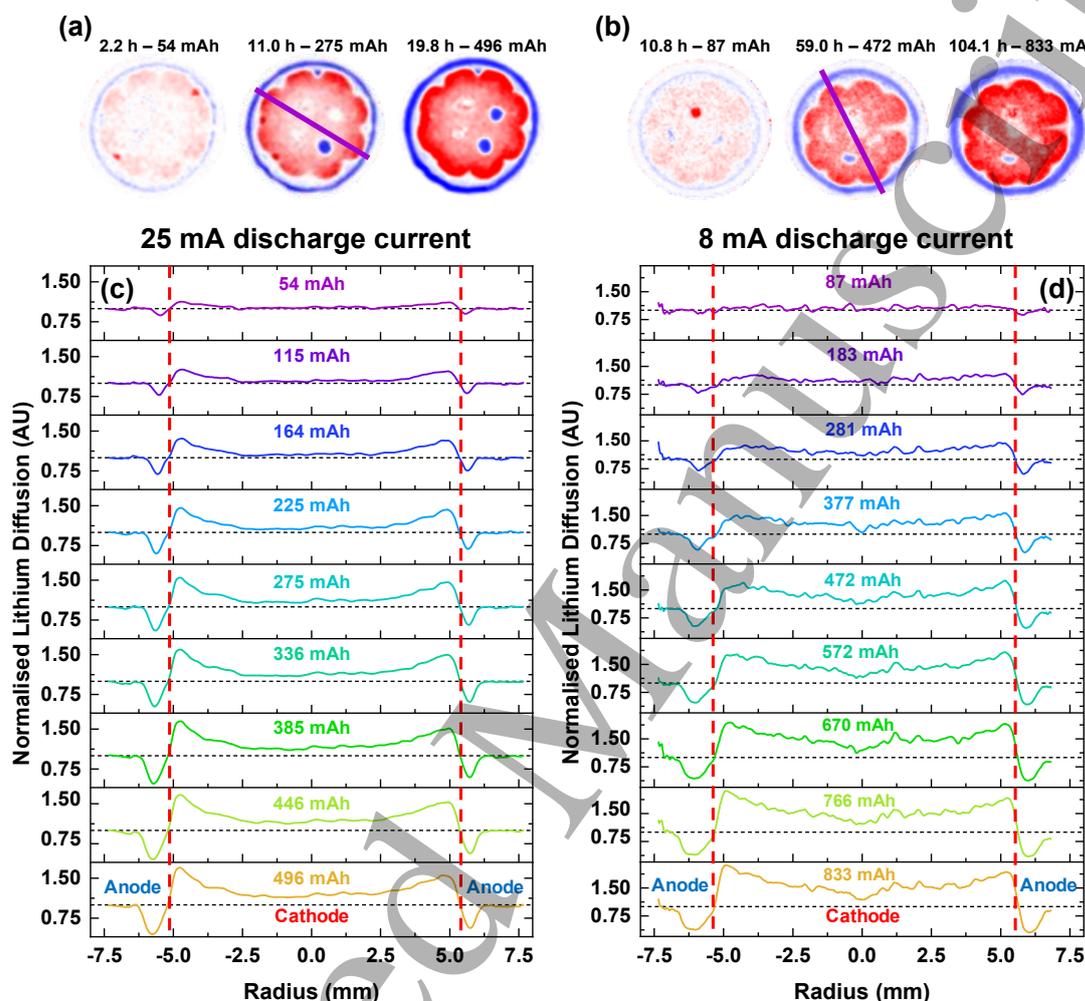
384 It can be seen that a Li removal rate of  $485 \text{ mm}^3 \text{ Ah}^{-1}$  is theoretically required for a  $\text{Li}/\text{SOCl}_2$   
 385 cell which corresponds to a minimum initial Li volume of  $582 \text{ mm}^3$ , or mass of  $0.31 \text{ g}$ , for the  
 386 cells examined in this work. By comparing this to the measured volumes it can be seen that in  
 387 this case the significant majority of the anode must be consumed to deliver the rated  $1.2 \text{ Ah}$   
 388 capacity. Experimentally determined Li removal rates can be calculated by interrogating the  
 389 slope of the curves shown in Figure 7. Here it is shown that  $514 \text{ mm}^3 \text{ Ah}^{-1}$  and  $462 \text{ mm}^3 \text{ Ah}^{-1}$   
 390 are required for the cells discharged at  $25 \text{ mA}$  and  $8 \text{ mA}$ , respectively. The discrepancy between the  
 391 values for the two cells can be explained by different thresholds for the volume segmentation  
 392 arising from the different neutron spectra of CONRAD-2 and IMAT which result in different  
 393 average attenuation coefficients for Li. Further, a slightly different utilised threshold can affect  
 394 a deviation of several cubic millimetres as well as the relative big pixel sizes which can lead to  
 395 a slightly higher or lower determined lithium volume. To provide a more representative  
 396 comparison with this theoretical value it is beneficial to use the mean of  $488 \text{ mm}^3 \text{ Ah}^{-1}$  of the  
 397 two measured values.



398  
 399 **Figure 7: Lithium volume decrease of the LS14250 anode during a discharge current of (a) 25 mA and (b) 8 mA, respectively. The**  
 400 **deviations from the expected linear volume reduction are due to variations in the segmentation process. The total error of the lithium**  
 401 **volume determination is estimated to be smaller than 5 %.**

402  
 403 A considerable drawback of the  $\text{SOCl}_2$  electrode chemistry is the slow Li diffusion inside the  
 404 cathode which can result in blocking of the diffusion channels in the carbon support skeleton  
 405 by the formation of solid sulphur from the chemical reaction with lithium. Quantification of  
 406 this can be achieved by examining changes in intensity, which indicates the Li diffusion  
 407 throughout the cell. Figure 8(c, d) shows profiles of the intensity through the reconstructed

408 slices of the anode and cathode for both the cell discharged at 25 mA and 8 mA. For the line  
 409 profiles a single horizontal orthogonal slice was used, which is the most representative for the  
 410 battery cell respectively, shown in Figure 8(a, b). A high lithium mobility can be seen at the  
 411 cathode edges over the discharge time for both cells, with the 25 mA discharged cell showing  
 412 a higher mobility as a result of the increased discharge current [Figure 8(c, d)].



413  
 414 Figure 8: Normalised grey values representing lithium redistributions inside the LS14250 battery cell during a discharge current of –  
 415 (a, c) 25 mA and (b, d) 8 mA. (a, b) selected horizontal slices from the middle part of the cell at different SoCs highlighting lithium  
 416 removal and accumulation. (c, d) time dependent line plots through the middle section of a LS14250 Li/SOCl<sub>2</sub> cell during the  
 417 discharging process. Values above the baseline indicate an increase of lithium in the cathode, and values below the baseline indicate  
 418 lithium removal from the anode.

419 The x-axis shows the radial distance from the centre of the cell, and the y-axis the relative  
 420 change of the lithium distribution in terms of greyscale values normalised to the initial SoC.  
 421 Values above the baseline are attributable to an increased lithium content (such as that observed  
 422 in the SOCl<sub>2</sub> electrode), with reductions in intensity associated with a decrease of lithium  
 423 concentration (as seen in the lithium metal anode). The low lithium amount in the inner cathode  
 424 region, shown by a trough in intensity towards the centre of the cell indicates a substantial

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3 425 stagnation in the lithium diffusion at a 25 mA discharge current. Figure 8(a) shows related  
4 426 horizontal slices where blue and red colours indicate the lithium removal and deposition,  
5 427 respectively. A high lithium accumulation at the bulges of the ‘flower’ shaped cathode  
6 428 boundary is clearly visible during the first discharge phase due to the favourable short distance  
7 429 between the lithium metal anode and the cathode. At the end of the discharging process, the  
8 430 red ring along the cathode border indicates high accumulation of lithium in contrast to the inner  
9 431 cathode region which is almost devoid of lithium. It should be noted that the blue coloured,  
10 432 circular regions inside the cathode are related to intensity changes in the reconstructions caused  
11 433 by the generation of  $\text{SO}_2$  gas which fill the gas channels, displacing the  $\text{SOCl}_2$  and causing a  
12 434 similar behaviour to that observed during Li removal from the anode. White areas represent no  
13 435 intensity changes during the discharging process which indicates regions with constant lithium  
14 436 amounts or regions unaffected by the reaction.

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16 437 Figure 8(b, d) shows a similar analysis for the cell discharged at 8 mA. In this case, the line  
17 438 profile plot shows a more equal Li distribution from the outer cathode edge to the centre of the  
18 439 cell. The lower discharge current facilitates improved Li diffusion properties due to the reduced  
19 440 reaction rate. The improved ratio can be seen by the higher lithium amount in the centre of the  
20 441 cathode in comparison to the cell discharged at 25 mA. The horizontal slices in Figure 8(b)  
21 442 also show a more homogeneous lithium distribution during the discharge before the  
22 443 concentration increases on the cathode border due to blocking effects in the carbon skeleton.  
23 444 This comparison of the time dependent lithium distributions inside the  $\text{SOCl}_2$  electrode reveals  
24 445 the major reason for the capacity loss with discharge at higher currents. The loss of usable cell  
25 446 capacity is strongly correlated to the rate of the lithium diffusion inside the cathode. Higher  
26 447 currents force the chemical reaction between the Li and the thionyl chloride whereby solid  
27 448 sulphur is formed impeding the diffusion channels of the porous supporting carbon skeleton  
28 449 and reducing the rate of Li diffusion. As a consequence, fresh unreacted  $\text{SOCl}_2$ , stored in the  
29 450 inner cathode region, cannot participate in the reaction.

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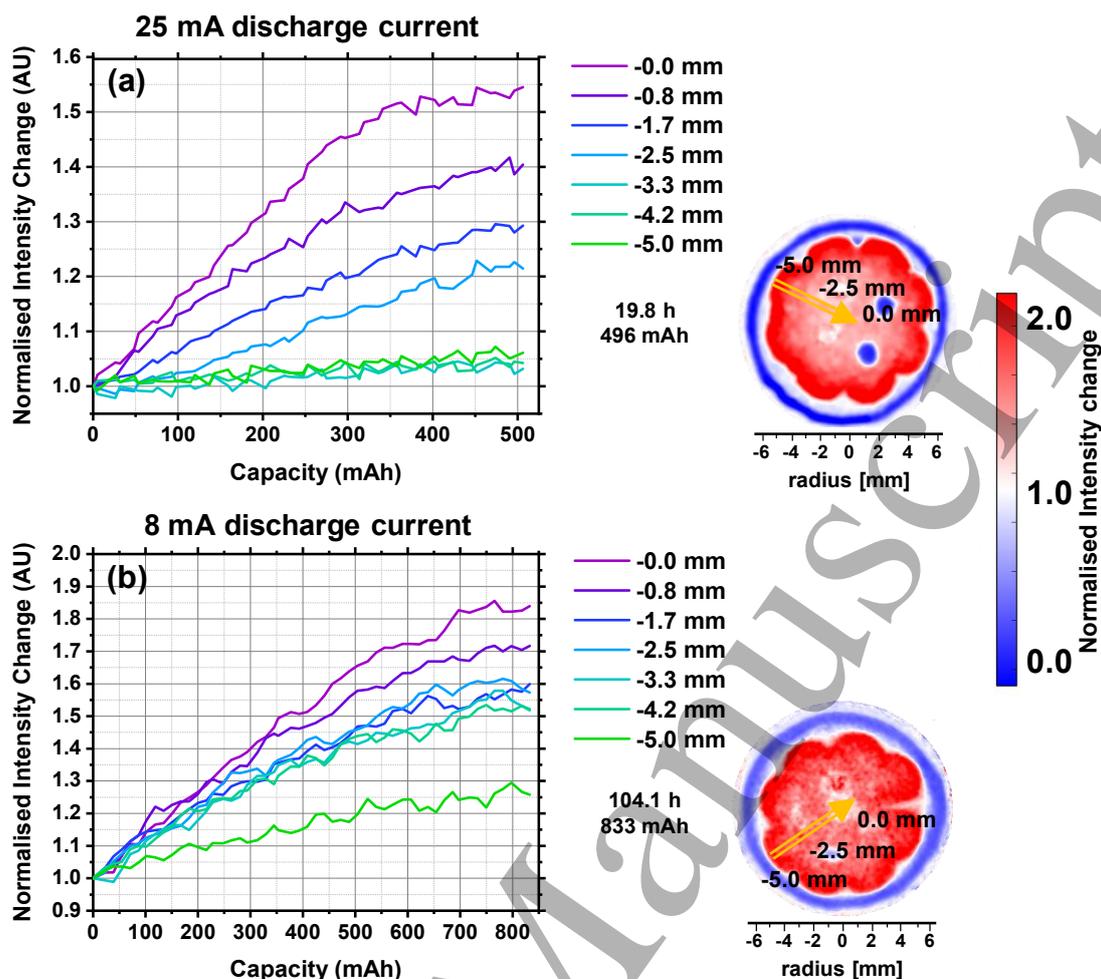
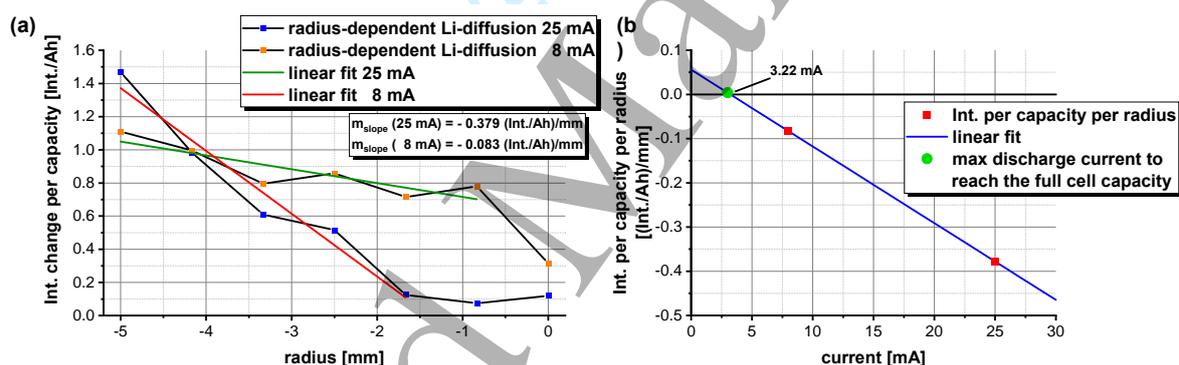


Figure 9: Relative grey value changes representing lithium diffusion inside the  $\text{SOCl}_2$  cathode at (a) 25 mA and (b) 8 mA alongside horizontal slices from the middle of the cell, with the yellow arrow pointing along the selected analysis points.

To better understand the problem of capacity loss at higher discharge rates, an improved understanding of the lithium diffusion process in the cathode is necessary with results detailed in Figure 9 in which the time dependent normalised intensity change at seven different positions, starting at the cathode edge and evenly distributed regions along the arrow towards the centre, is measured in the most representative horizontal slices for both discharge rates. The detected normalised intensity can be interpreted as a measure of the quantity of Li present at any given position. Figure 9(a) presents the normalised intensity change from a radial distance of -5.0 to 0.0 mm for the cell discharged at 25 mA. The values were determined along a representative line which is shown in the orthoslice at different distances from the cathode centre. The line was placed in such a way that the gas channels do not influence the measurement result. The results shown in Figure 9(a) indicate an increased level of lithium at a radius of -5.0 mm, which steadily decreases through the cell to a boundary located at a radius of ca. -2.5 mm, beyond which no lithium is seen to diffuse. Above approximately 350 mAh, the lithium diffusion at the outer cathode part can be seen to plateau, indicating a saturation of the cathode. However,

468 due to the constant current discharge this stagnation of the Li diffusion must be compensated  
 469 by an increased rate of Li diffusion elsewhere. It is likely that this happens in the gaps between  
 470 the ‘flowery’ bulges at the cathode boundary, which are more active than other regions during  
 471 the initial part of discharge process owing to the shorter diffusion paths for the Li-ions from  
 472 anode to cathode. The rate of Li diffusion seems to only stagnate in the outer cathode region  
 473 (–5.0 mm) with an increase in intensity, and consequently continued diffusion, evident in the  
 474 inner regions (–4.2 mm to –2.5 mm) suggesting that the limitation on the capacity provided by  
 475 the cell occurs in the outer cathode shell area.

476 At a lower discharge current, the lithium diffusion inside the cathode is slightly more  
 477 homogeneous with a noticeable decrease inwards the cathode. Figure 9(b) shows the lithium  
 478 diffusion behaviour inside the  $\text{SOCl}_2$  cathode for the cell discharged at 8 mA. In contrast to the  
 479 higher discharge current of 25 mA, the rate of intensity rise is consistent across all regions,  
 480 with the internal regions displaying a substantially increased change in intensity. These findings  
 481 demonstrate the mechanisms behind the improved capacity provided by lower operating  
 482 currents, which enables Li diffusion deeper inside the cathode enabling use of more unreacted  
 483  $\text{SOCl}_2$ .



484  
 485 **Figure 10: Determination of the intensity/lithium amount change per cell capacity and the maximal discharge current which allows**  
 486 **for the use of the full cell capacity showing (a) the observed intensity change, and the calculated slopes for the cells discharged at**  
 487 **25 mA and 8 mA and (b) an estimation of the maximal usable discharge current to reach the full cell capacity occurring at the**  
 488 **intersection of the curve with the abscissa.**

489 The spatially variant intensity increase per capacity is a useful metric to compare the Li  
 490 diffusion behaviour inside the cathode for different discharge currents. The intensity-capacity  
 491 slopes for the graphs plotted in Figure 9 are displayed over the cathode radial distance in Figure  
 492 10. The slope values over the radial distance show a linear decrease of Li diffusion, with an  
 493 increased rate observed for the cell discharged at 25 mA scan due to higher Li use. At a radius  
 494 of about –1.5 mm the lithium diffusion seems to stop while the cell discharged at 8 mA shows  
 495 evidence of Li diffusion throughout the entire cell. The point shown at 0.0 mm includes a small  
 496 contribution in intensity of the cathode current collector which causes a slightly elevated

change. A fit of the slope of the linear region is a measure of the capacity and radius dependent Li diffusion which is  $-0.379$  (Int Ah<sup>-1</sup>) mm<sup>-1</sup> for the cell discharged at 25 mA and  $-0.083$  (Int Ah<sup>-1</sup>) mm<sup>-1</sup> for that at 8 mA. From the slope it is possible to determine a maximum discharge current which enables the full capacity to be utilised. The Li diffusion per capacity and radius is plotted over the discharge current in Figure 10 b). Assuming a linear dependence for both values, the abscissa-axis intersection represents the maximal discharge current to reach the full cell capacity and is marked with a green dot which corresponds to approximately 3.2 mA. This maximum cell utilisation rate is an order of magnitude lower than the maximum recommended continuous current of 35 mA and demonstrates the capacity limitation encountered at maximum discharge rate.

### Conclusions

Multi-modal tomography was performed using X-rays and neutrons to elucidate the dynamic processes which occur inside primary LiSOCl<sub>2</sub> cells during discharge. These complementary methods enable the visualisation of the changes which occur in the cell components due to the different attenuation characteristics in the two techniques. X-ray tomography identified the consumption of the SOCl<sub>2</sub> electrolyte, which resulted in the evolution of SO<sub>2</sub> gas; however no significant structural deformations were observed using this method. In contrast, neutron imaging enabled the identification of the rate dependent diffusion characteristics of Li within the cell. Time dependent neutron tomography was enabled through the use of the golden ratio imaging technique, which substantially improves the temporal resolution of the imaging process, even at low flux neutron sources. The gas evolved during discharge was found to inhibit the performance by isolating regions of Li. Furthermore, the rate of Li diffusion was observed to be spatially variable, with regions identified where the diffusion process was seen to stagnate during discharge.

The two imaging methods have provided an improved understanding of the performance of the cells. Where X-rays are more sensitive to metallic cell components such as the battery casing or the current collectors, neutrons visualise inter alia the lithium diffusion. The combination of both techniques helps to understand processes which are hidden for one technique or localise battery components, such as the cathode current collector in the cell centre, which are invisible for neutrons but the location is important for the analysis. For the discharge currents used in this study, the capacity of the cells was observed to fall significantly short of the nominal capacity, due to the slow lithium diffusion and the presence of unusable lithium. This bobbin type cell design shows significant radial disparity in the rate of Li diffusion at higher discharge rates suggesting a need to either limit the maximum current drawn from the cell or amend the cell design to promote improved Li diffusion. A calculation to determine the maximum capacity

with this cell design suggests that the discharge rate (to ensure maximum capacity) should be at least an order of magnitude lower than the maximum current suggested by the manufacturer.

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